MEMORANDUM

July 5, 2019

TO: Historical Memo

FM: Peter Carter / Steven Yee

RE: Carnation Wastewater Treatment Plant

June 2019 Process Summary

The Carnation Treatment Plant (CTP) discharged to the Chinook Bend wetlands for the entire month of June. Effluent Biochemical Oxygen Demand (BOD₅) and Total Suspended Solids (TSS) averaged <1.3 mg/L and <2.0 mg/L, respectively. BOD₅ and TSS removals were both >99%. All permit-required samples were collected and analyzed. Effluent flow averaged 0.104-MGD. Influent flow to the CTP averaged slightly higher (0.110-MGD) due to internal recycle flows. The max-day effluent flow was 0.120-MGD on June 2. The permeate temperature ranged from $71^{\circ}F$ to $75^{\circ}F$ across the month.

The plant operated with one of two aeration basins in service (Basin 1). The MLSS averaged 8640-mg/L. An estimated 7170 dry lbs. of waste sludge and scum were hauled to the South Plant for further treatment. Flow was cycled through all five membrane trains and both UV trains in June.

Total-N removal averaged 90%. Effluent ammonia (NH₃) averaged <0.1-mg/L as N. Effluent nitrite plus nitrate (NO₂+NO₃) averaged 5.3-mg/L as N. Total phosphorus (P) averaged 3.3-mg/L for a total P removal of 60%. N and P analyses are performed on a weekly basis.

Alkalinity was added to the secondary process to always maintain the effluent pH above pH 6.8. Caustic Soda (25% solution) was the alkalinity source this month; a total of 554 gallons was used. Effluent alkalinity averaged 137-mg/L (with a range of 125-146) as CaCO₃; influent alkalinity was in the range of 222-279 mg/l as CaCO₃. Alkalinity addition replaces the alkalinity lost during nitrification; the effluent pH would likely fall below the permitted minimum pH 6.0 if alkalinity addition stopped.

Tables 1 and 2 present membrane maintenance cleaning information and membrane performance data, respectively. Average TMPs were in the 1.5 to 1.6 psi range. The control system limits flow through the membranes to keep the TMP <8.0-psi; this protects the membranes' integrity. An estimated 65-gallons of 12.5% sodium hypochlorite were used for maintenance cleans in June.

Table 1: Membrane Maintenance Cleans Performed

Week Beginning	Train 1	Train 2	Train 3	Train 4	Train 5
6/1	MC ¹	MC	MC	MC	MC
6/8	MC	MC	MC	MC	MC
6/15	MC	MC	MC		MC
6/22	MC	MC	MC	MC	MC

¹ MC refers to a maintenance clean

Table 2: Membrane Performance June 2019

MEMBRANE PARAMETERS	Train 1	Train 2	Train 3	Train 4	Train 5
Permeate Turbidity (NTU) ¹					
Average for Month	0.08	0.09	0.06	0.08	0.08
Design	< 0.2	< 0.2	< 0.2	< 0.2	< 0.2
Permeate Flow (GPD) ²					
Average Daily for Month	22,366	25,652	23,912	24,365	24,517
AADF (Annual Average Flow) Design	97,500	97,500	97,500	97,500	97,500
Maximum Daily for Month	41,228	38,641	33,705	38,180	42,456
PDF (Peak Day) Design	165,000	165,000	165,000	165,000	165,000
Permeate Flow Rate (GPM) ³					
Average for Month	18	19	17	18	19
Peak Hour for Month	106	90	88	101	88
PHF (Peak Hour) Design	180	180	180	180	180
Instantaneous Flux (GFD ⁴) ⁵					
Average for Month	7.2	6.9	7.5	7.3	7.2
Trans-Membrane Pressure (PSI) ⁶					
Average for Month	1.6	1.5	1.6	1.5	1.5
Maximum for Month	7.9	8.2	2.6	3.6	7.8
(Average/Maximum) Design	2.0/10	2.0/10	2.0/10	2.0/10	2.0/10
Permeate Temperature (°C) ⁷					
Minimum for Month	21.5	21.5	21.5	21.5	21.5
Design	>12	> 12	> 12	> 12	> 12
Permeability at 20°C (GFD/PSI) ⁸					
Average for Month	4.5	4.4	4.5	4.7	4.6
(Recovery Clean Trigger) Design	< 3.0	< 3.0	< 3.0	< 3.0	< 3.0

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¹ Permeate turbidity – indication of membrane integrity.

² Permeate flow – compares operating to design capacity. The design capacity (AADF and PDF) are both based on entire treatment plant flow with four membrane trains available.

³ Permeate flow rate – check of acute operating conditions to confirm peak hour design condition is not being approached. The design capacity (PHF) is based on entire treatment plant flow with five membrane trains available. The average rate is only for when the membrane is operating.

⁴ "GFD" is shorthand for "GPD/Ft²". GFD is a flux measurement based on the flow (gallons/day) of permeate that passes through a square foot of membrane surface. Each train has one membrane cassette with 12,920 square feet of surface area.

⁵Instantaneous flux – check of membrane operating flux. Instantaneous differs from net flux in that it does not account for backpulse and/or relax periods (It is therefore always slightly higher). The design condition is based on net flux and therefore not included. The permeate flow design conditions provide the same information since only a single cassette is operating in each membrane train.

⁶ Trans-membrane pressure – provides information related to fouling and biological process operation (MLSS and filterability). The average and maximum TMP are included for reference.

⁷ Permeate temperature – listed since the hydraulic capacity can be reduced when operating below the minimum design temperature (de-rating of membrane capacity).

⁸ Permeability (temperature corrected to 20°C) – parameter assesses fouled condition of membrane. The trigger value listed is from the GE O&M manual.